

# The Phase-field Modeling of Hydraulic Fracture

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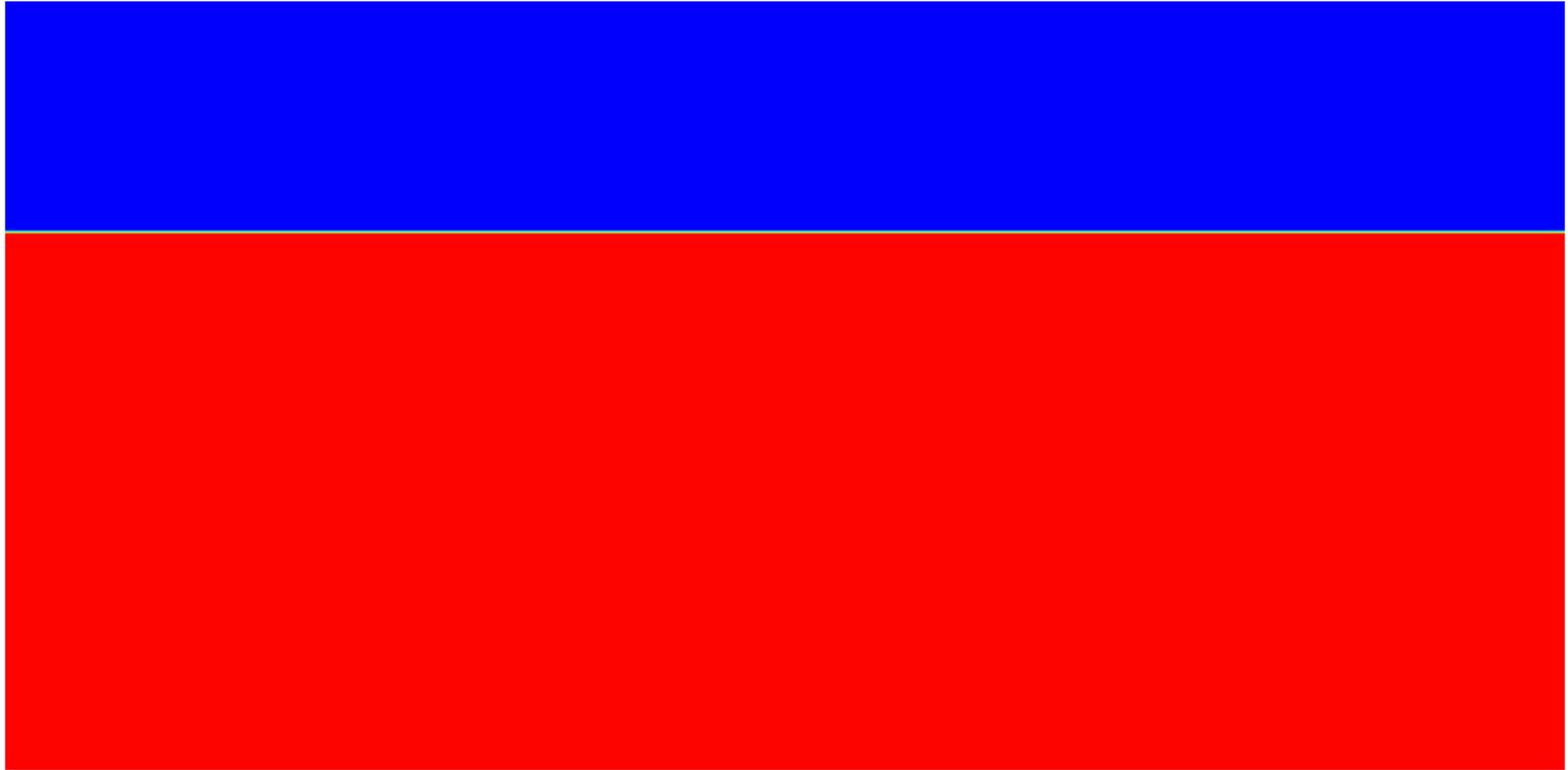
**Variational Models of Fracture**  
**Banff International Research Station**  
**for Mathematical Innovation and Discovery**  
**5/9/2016**



The University of Texas at Austin  
**Aerospace Engineering  
and Engineering Mechanics**  
*Cockrell School of Engineering*

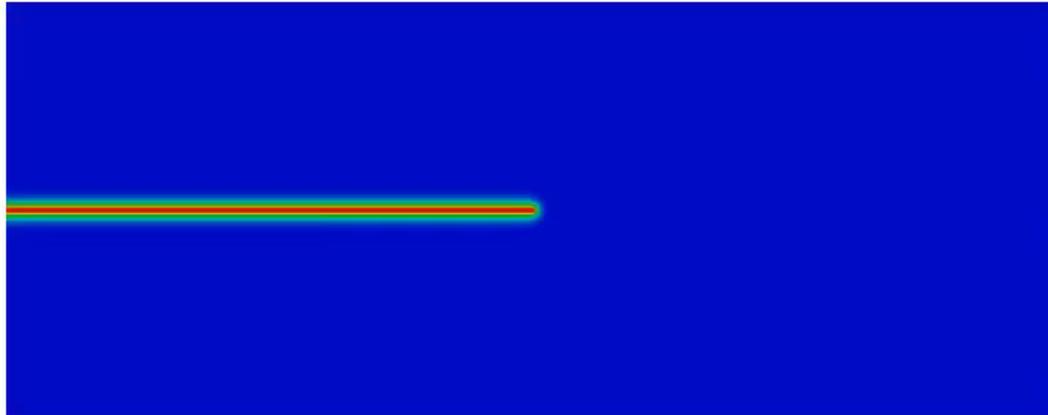
# Boiling

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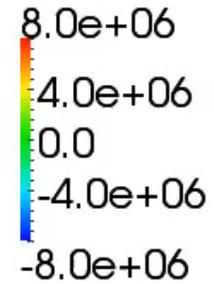


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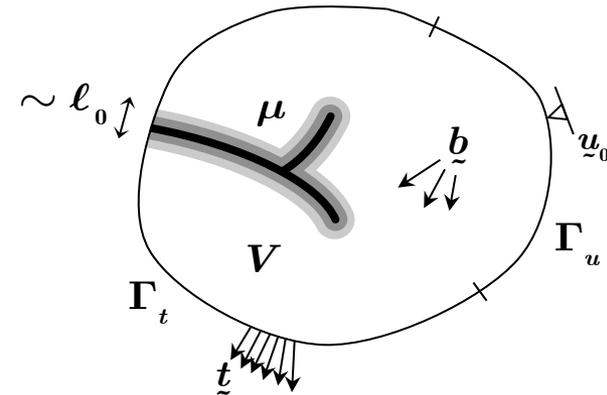
Hydrostatic Stress



# Micro-force Balance Approach

- $\lambda = \xi_i n_i$  - Externally applied surface micro-force  
 $\gamma$  - Externally applied body micro-force  
 $\pi$  - Internal micro-force per unit volume

$$\int_S \lambda dS + \int_V (\gamma + \pi) dV = 0 \quad \rightarrow \quad \xi_{i,i} + \pi + \gamma = 0$$



$$\text{1st Law} \quad \rightarrow \quad \frac{d}{dt} \int_V (\tilde{u} + \frac{1}{2} \rho v_i v_i) dV = \int_S \lambda \dot{\mu} dS + \int_V \gamma \dot{\mu} dV + \dots$$

$$\text{2nd Law analysis} \quad \rightarrow \quad \xi_i = \frac{\partial \psi}{\partial \mu_{,i}}, \quad \pi = -\frac{\partial \psi}{\partial \mu} - \beta \dot{\mu} \quad \rightarrow \quad \left( \frac{\partial \psi}{\partial \mu_{,i}} \right)_{,i} - \frac{\partial \psi}{\partial \mu} + \gamma = \beta \dot{\mu}$$

$$\psi(\varepsilon_{ij}, \mu, \mu_{,i}) = f_d(\mu) \psi^+ + \psi^- + \frac{G_c}{4\ell_0} (1 - \mu)^2 + G_c \ell_0 \mu_{,i} \mu_{,i}$$

# Degradation Function

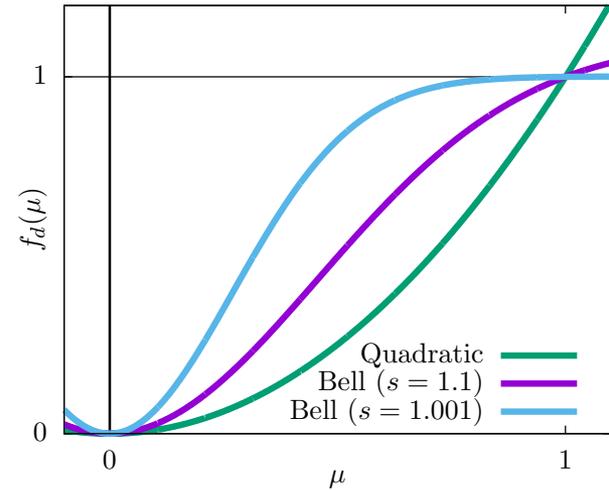
**LEFM:** 
$$\psi = f_d(\mu)\Omega^+ + \Omega^- + \frac{G_c}{4\ell_0}(1-\mu)^2 + G_c\ell_0\mu_{,i}\mu_{,i}$$

$$\Omega^+ = \frac{\bar{\lambda}}{2} \langle \varepsilon_{kk} \rangle^2 + \bar{\mu} \left( \langle \varepsilon_1 \rangle^2 + \langle \varepsilon_2 \rangle^2 + \langle \varepsilon_3 \rangle^2 \right)$$

$$\Omega^- = -\frac{\bar{\lambda}}{2} \langle -\varepsilon_{kk} \rangle^2 - \bar{\mu} \left( \langle -\varepsilon_1 \rangle^2 + \langle -\varepsilon_2 \rangle^2 + \langle -\varepsilon_3 \rangle^2 \right)$$

Requirements:

$$f_d(1) = 1, \quad f_d(0) = 0, \quad f_d'(0) = 0, \quad f_d \in C^1$$



Quadratic Form:

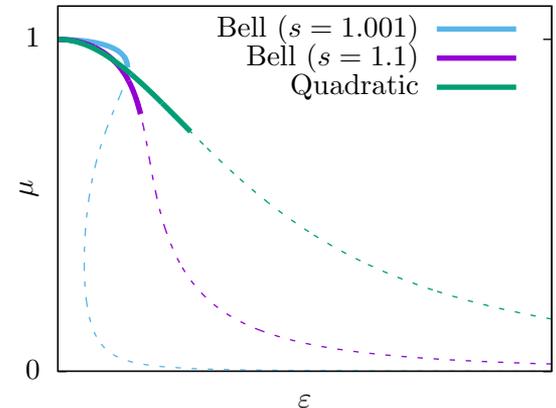
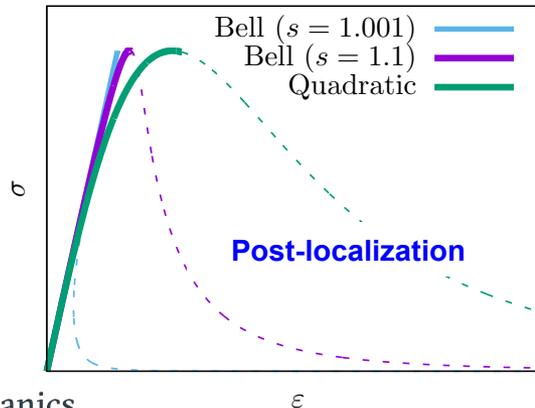
$$f_d(\mu) = \mu^2$$

Modified "Bell Curve" Form:

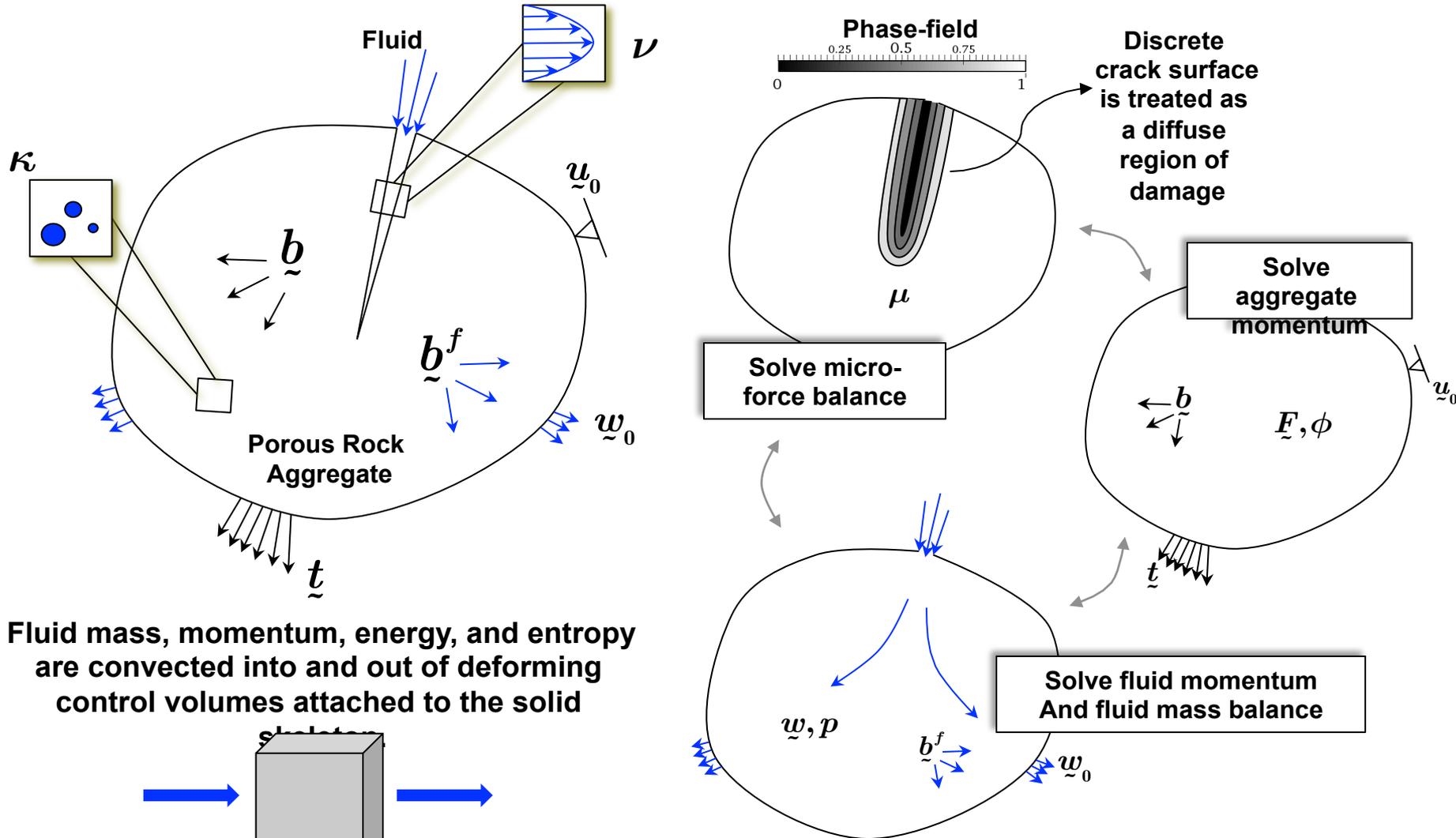
$$f_d(\mu) = s \left[ 1 - \left( \frac{s-1}{s} \right)^{\mu^2} \right]$$

Homogenous Stress-Strain Response

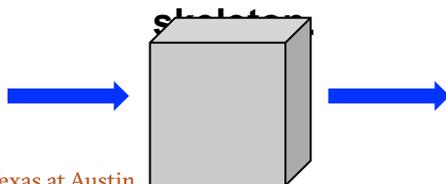
The length scale for each curve has been adjusted to yield the same peak stress



# Phase-field Approach to Hydraulic Fracture



Fluid mass, momentum, energy, and entropy are convected into and out of deforming control volumes attached to the solid



# Mass Balance

Solid mass balance: 
$$\frac{D}{Dt}[(1 - \phi)\rho^s J] = 0$$

Fluid mass balance: 
$$\frac{D}{Dt}[\phi\rho^f J + g_m(\mu)\rho^f(1 - \phi)\langle J - 1 \rangle] = -(\rho^f \tilde{w}_I)_{,I} + \rho^f \tilde{m}$$

$$g_m(\mu) = \begin{cases} 1 & ; \quad \mu < 0 \\ 1 - 3\mu^2 + 2\mu^3 & ; \quad 0 \leq \mu \leq 1 \\ 0 & ; \quad \mu > 1 \end{cases}$$

Effective porosity: 
$$\bar{\phi} = \phi + g_m(\mu)(1 - \phi)\langle J - 1 \rangle \frac{1}{J}$$

Fluid mass balance  $\Rightarrow$  
$$\frac{D}{Dt}[\rho^f \bar{\phi} J] = -(\rho^f \tilde{w}_I)_{,I} + \rho^f \tilde{m}$$

$\phi \equiv$  porosity

$\rho^s, \rho^f \equiv$  solid and fluid densities

$\mu \equiv$  phase-field parameter

$J \equiv$  determinant of the deformation gradient  $F_{iJ}$

$\tilde{w}_I \equiv$  nominal fluid flux  $\left( w_i = \frac{\tilde{w}_K F_{iK}}{J} \right)$

$\tilde{m} \equiv$  fluid volume injected per unit reference volume

# Momentum and Micro-force Balances

$$\text{Effective porosity: } \bar{\phi} = \phi + g_m(\mu)(1 - \phi) \langle J - 1 \rangle \frac{1}{J}$$

$$\text{Aggregate momentum: } P_{Ki,K} + \tilde{b}_i = (1 - \phi)\rho^s J \dot{v}_i + \bar{\phi}\rho^f J \dot{(v_i + v_i^{f/s})} + \bar{\phi}\rho^f J (v_i + v_i^{f/s})_{,K} F_{Kj}^{-1} v_j^{f/s}$$

$$\text{Fluid momentum: } (\bar{\phi} T_{Ji})_{,J} + \tilde{b}_i^f + \tilde{f}_i^{sf} = \bar{\phi}\rho^f J \dot{(v_i + v_i^{f/s})} + \bar{\phi}\rho^f J (v_i + v_i^{f/s})_{,K} F_{Kj}^{-1} v_j^{f/s} \quad (\text{Navier-Stokes})$$

$$\text{Solid momentum: } \underbrace{(P_{Ji} - \bar{\phi} T_{Ji})_{,J}}_{[(1 - \phi)P_{Ji}^s]_{,J}} + \tilde{b}_i^s - \tilde{f}_i^{sf} = (1 - \phi)J\rho^s \dot{v}_i \quad (\text{Newton's 2nd Law for the Solid})$$

$$\text{Micro-force balance: } \tilde{\xi}_{I,I} + \tilde{\gamma} + \tilde{\pi} = 0 \quad (\text{Governs changes and evolution of the phase-field})$$

$$v_i = \frac{D}{Dt} [u_i] \equiv \text{velocity of the aggregate}$$

$$\frac{w_i}{\phi} = v_i^{f/s} \equiv \text{average fluid velocity relative to the aggregate}$$

$$P_{Ji} \equiv \text{1st Piola-Kirchhoff stress for aggregate}$$

$$(\tau_{ji} - p\delta_{ij})JF_{Kj}^{-1} = T_{Ki} \equiv \text{1st Piola-Kirchhoff stress for the fluid}$$

# A Biot-type Formulation with Phase-field

$$(1 - \phi_0) J_0 \rho_0^s \Omega^s = g_d(\mu) \Omega^+(F_{iJ}) + \Omega^-(F_{iJ}) - \left(1 - g_m(\mu) \langle J - 1 \rangle^0\right) \left( \alpha (J - 1) p + \frac{1}{2M} p^2 \right) + \frac{G_c}{4\ell_0} \left[ (1 - \mu)^2 + 4\ell_0^2 \mu_{,I} \mu_{,I} \right]$$

Constitutive equations developed using the First and Second Laws of Thermodynamics

$$\phi J = \frac{1 - g_m(\mu) \langle J - 1 \rangle^0}{1 - \left(\frac{1}{J}\right) g_m(\mu) \langle J - 1 \rangle} \left( \alpha (J - 1) + \frac{p}{M} \right)$$

$$P_{Ji} = f_d(\mu) \frac{\partial \Omega^+}{\partial F_{iJ}} + \frac{\partial \Omega^-}{\partial F_{iJ}} - \left[ \alpha + g_m(\mu) \langle J - 1 \rangle^0 (1 - \alpha) \right] J F_{Ji}^{-1} p + \bar{\Phi} \tilde{\tau}_{Ji}$$

$$\tilde{\pi} = -g_d'(\mu) \Omega^+(F_{iJ}) + \frac{G_c}{2\ell_0} (1 - \mu) + g_m'(\mu) \left[ (1 - \alpha) \langle J - 1 \rangle p - \frac{1}{2M} \langle J - 1 \rangle^0 p^2 \right]$$

$$\tilde{\xi}_I = 2G_c \ell_0 \mu_{,I}$$

# Reduced Fluid Momentum (Brinkman Equation)

Low Reynolds Number Flow  
(inertial terms are neglected)

$$(\bar{\phi} T_{Ji})_{,J} + \tilde{b}_i^f + \tilde{f}_i^{sf} = 0$$

Linearized Compressibility

$$\psi^f = \frac{1}{c^f} \left( \frac{\rho_0^f}{\rho^f} + \ln(\rho^f) \right)$$

$$p = (\rho^f)^2 \frac{\partial \psi^f}{\partial \rho^f} \Rightarrow \rho^f = \rho_0^f + c^f p$$

Constitutive relations satisfying the  
dissipation inequality for the fluid

$$\tau_{ij} = g_S(\mu) \nu \left[ w_{i,j} + w_{j,i} - \frac{1}{3} w_{k,k} + \bar{\phi} \left( v_{i,j} + v_{j,i} - \frac{1}{3} v_{k,k} \right) \right]$$

$$T_{Ji} = (\tau_{ji} - p \delta_{ij}) J F_{Jj}^{-1}$$

$$g_S(0) = 1, \quad g_S(1) = 0$$

$$g_D(0) = 0, \quad g_D(1) = 1$$

$$\tilde{f}_i^{sf} = p \left( \bar{\phi} J F_{Ji}^{-1} \right)_{,J} - \bar{\phi}_{,J} \tilde{\tau}_{Ji} - g_D(\mu) \bar{\phi} J \frac{\nu}{\kappa} w_i$$

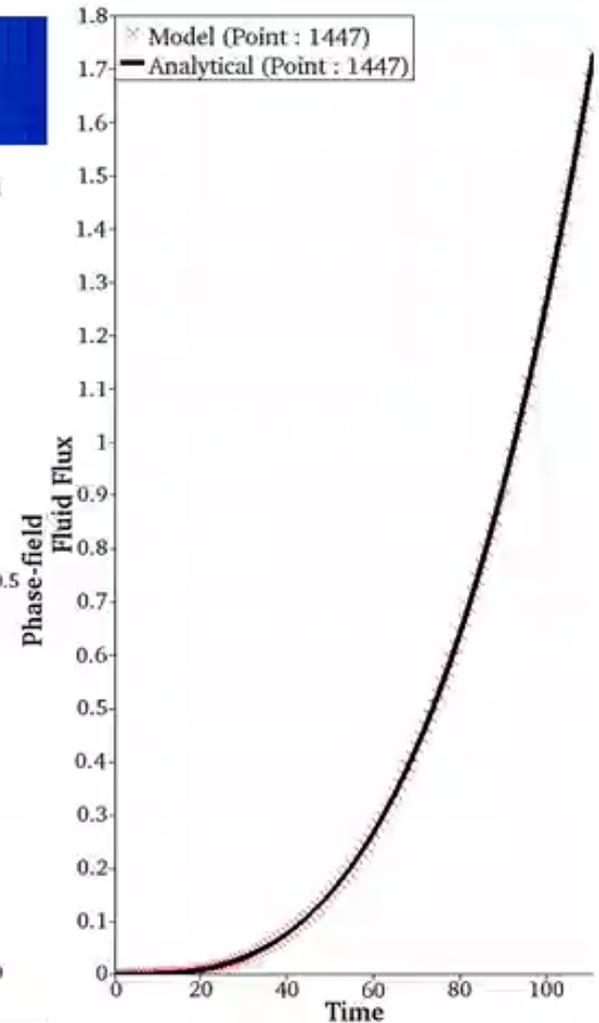
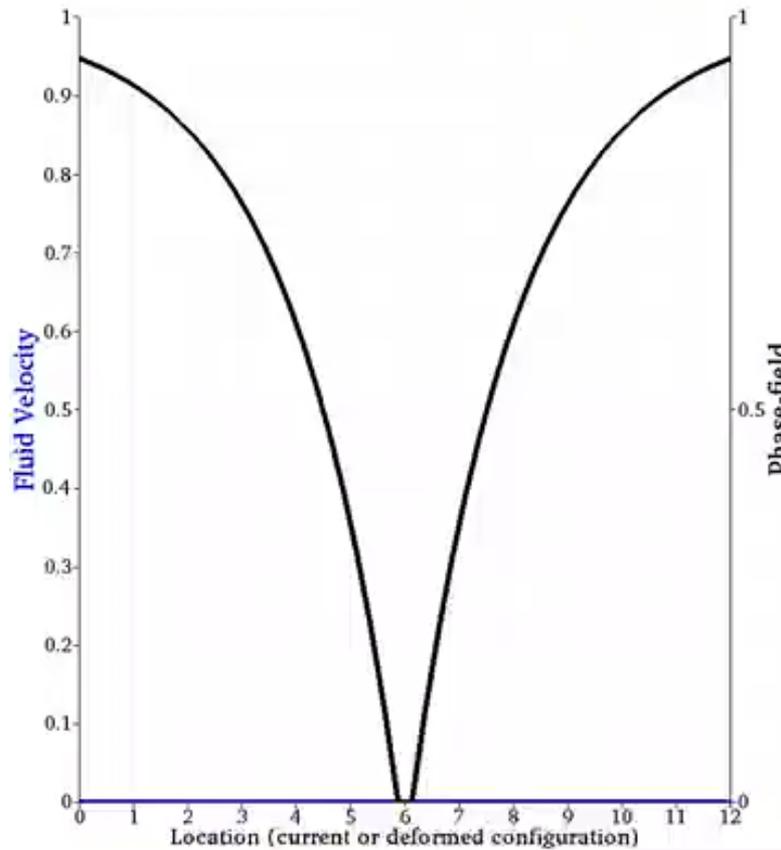
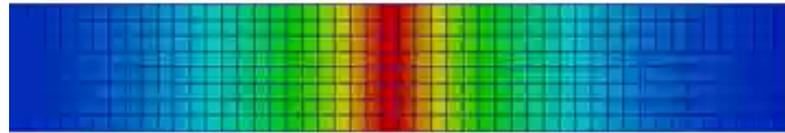
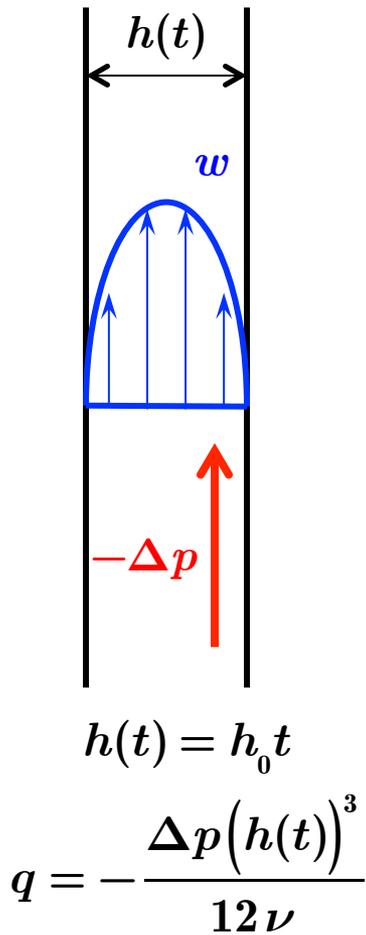
$$\Rightarrow \left( \tau_{ji} J F_{Jj}^{-1} \right)_{,J} - J F_{Ji}^{-1} p_{,J} - J g_D(\mu) \frac{\nu_{isc}}{\kappa} w_i + \tilde{b}_i^f = 0$$

Stokes flow when  $\mu=0$

Darcy flow when  $\mu=1$

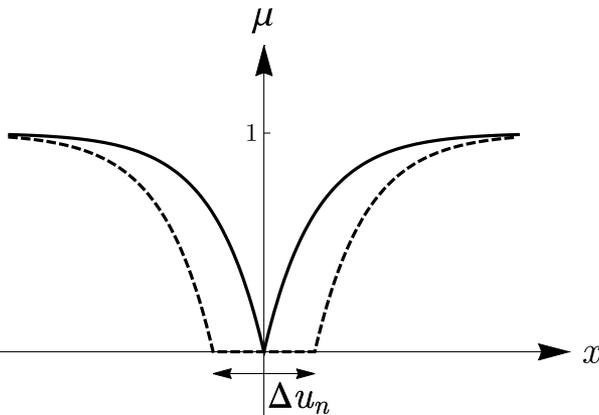
# Numerical Results and Validation

# Flow Through an Opening Channel

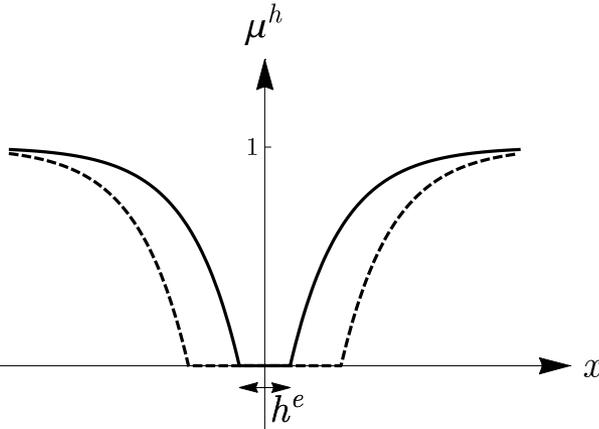


# Viscosity Scaling

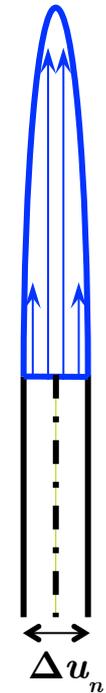
Exact Solution



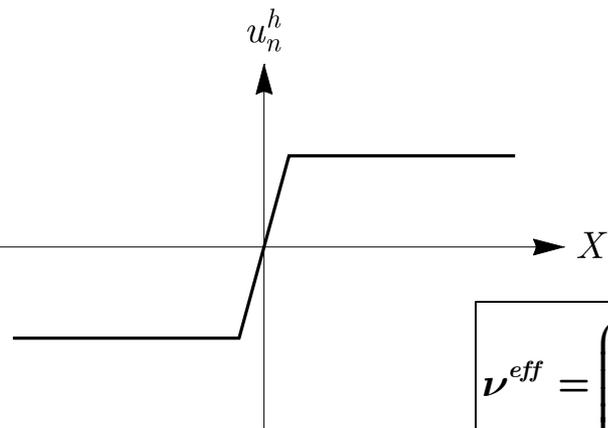
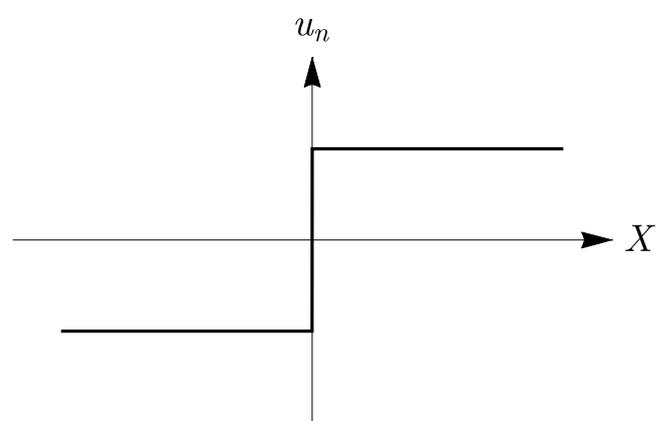
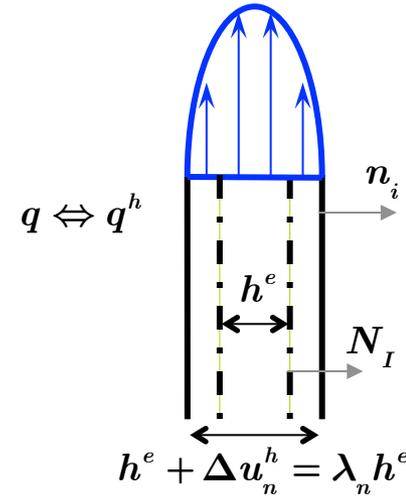
Numerical Solution



Exact Solution



Numerical Solution



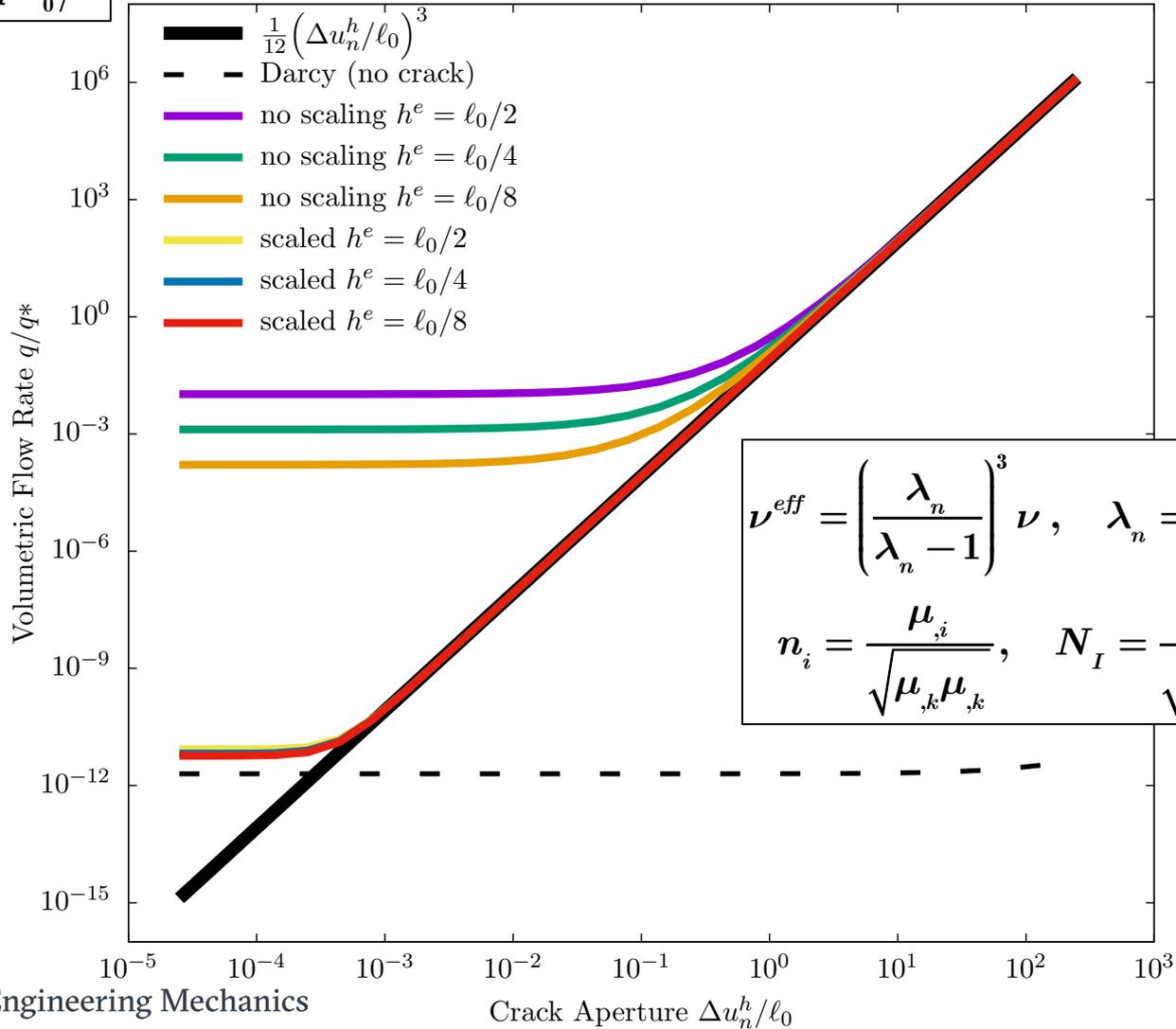
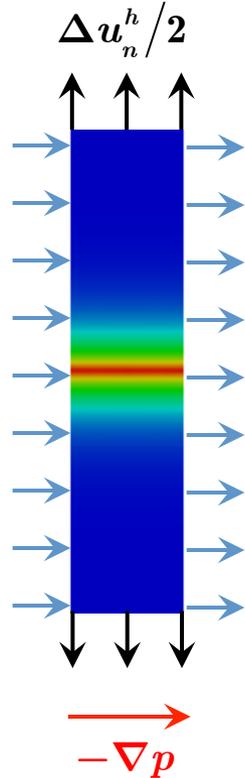
$$\nu^{eff} = \left( \frac{\lambda_n}{\lambda_n - 1} \right)^3 \nu, \quad \lambda_n = F_{i,j} n_i N_j$$

$$n_i = \frac{\mu_{,i}}{\sqrt{\mu_{,k} \mu_{,k}}}, \quad N_I = \frac{\mu_{,I}}{\sqrt{\mu_{,K} \mu_{,K}}}$$

# Viscosity Scaling

$$q^* = -\nabla p \ell_0^3 / \nu$$

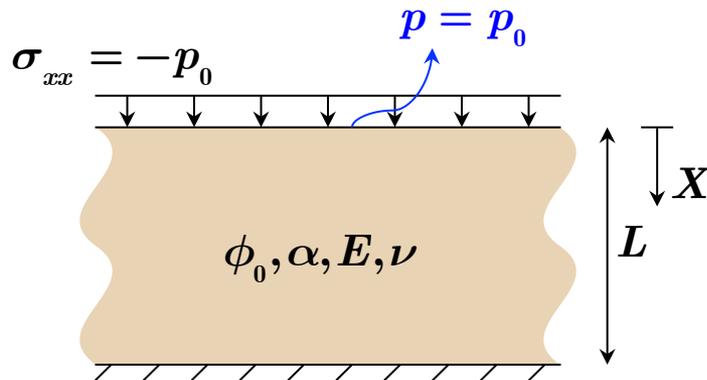
Total Flux vs. Crack Aperture ( $\kappa/\ell_0^2 = 10^{-14}$ )



$$\nu^{eff} = \left( \frac{\lambda_n}{\lambda_n - 1} \right)^3 \nu, \quad \lambda_n = F_{iJ} n_i N_J$$

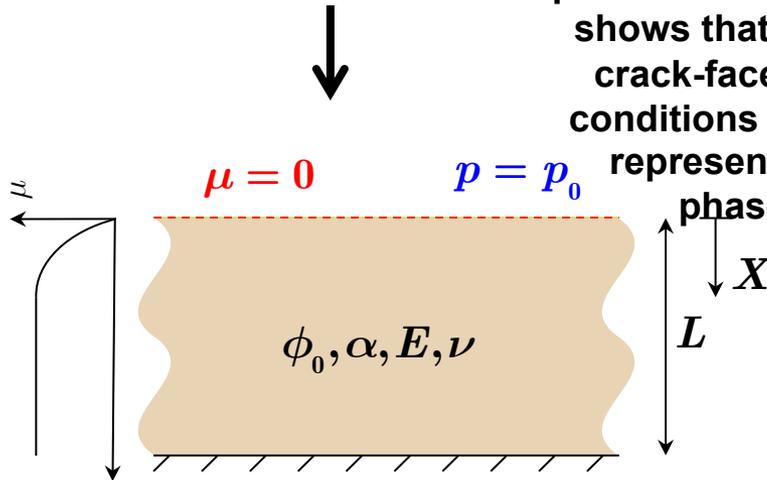
$$n_i = \frac{\mu_i}{\sqrt{\mu_{,k} \mu_{,k}}}, \quad N_I = \frac{\mu_{,I}}{\sqrt{\mu_{,K} \mu_{,K}}}$$

# Consolidation with Fluid Loading

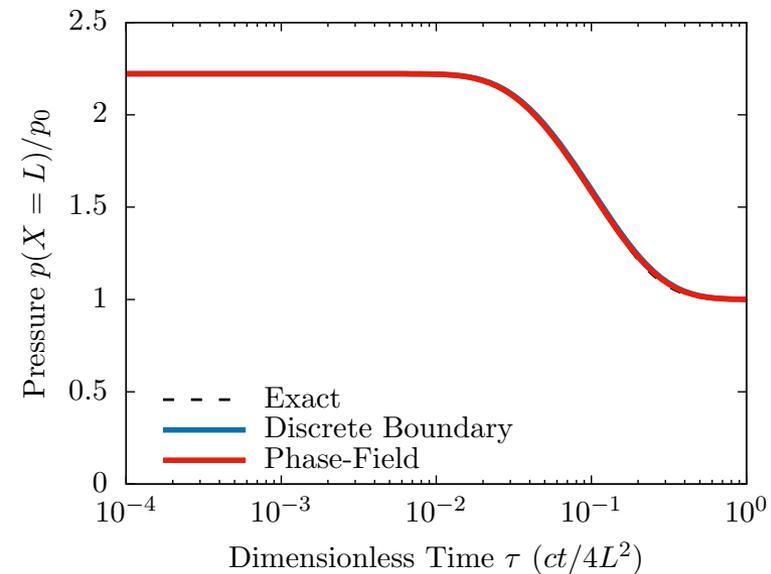
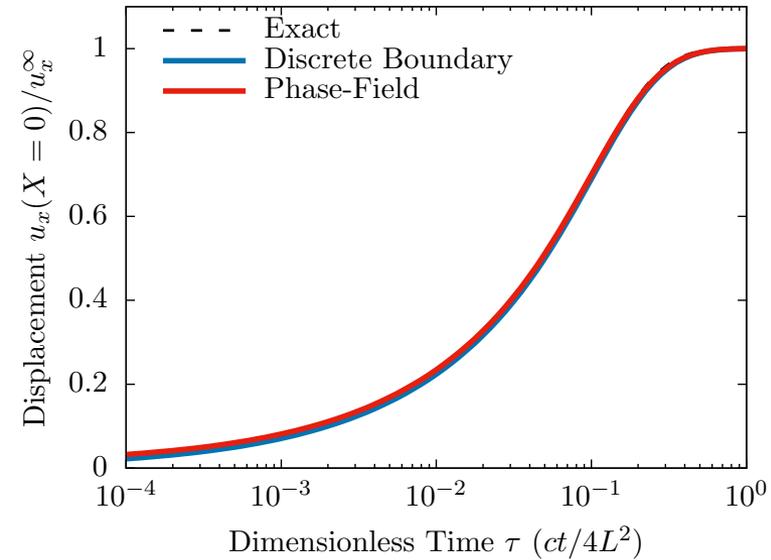


$u_x = 0$     $w_x = 0$

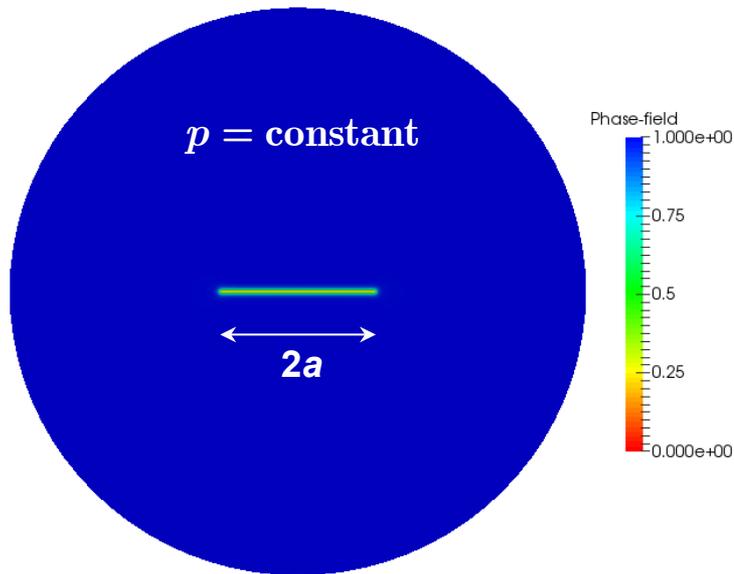
The top surface is represented by the phase-field. This solution shows that poroelastic crack-face boundary conditions are properly represented by the phase-field.



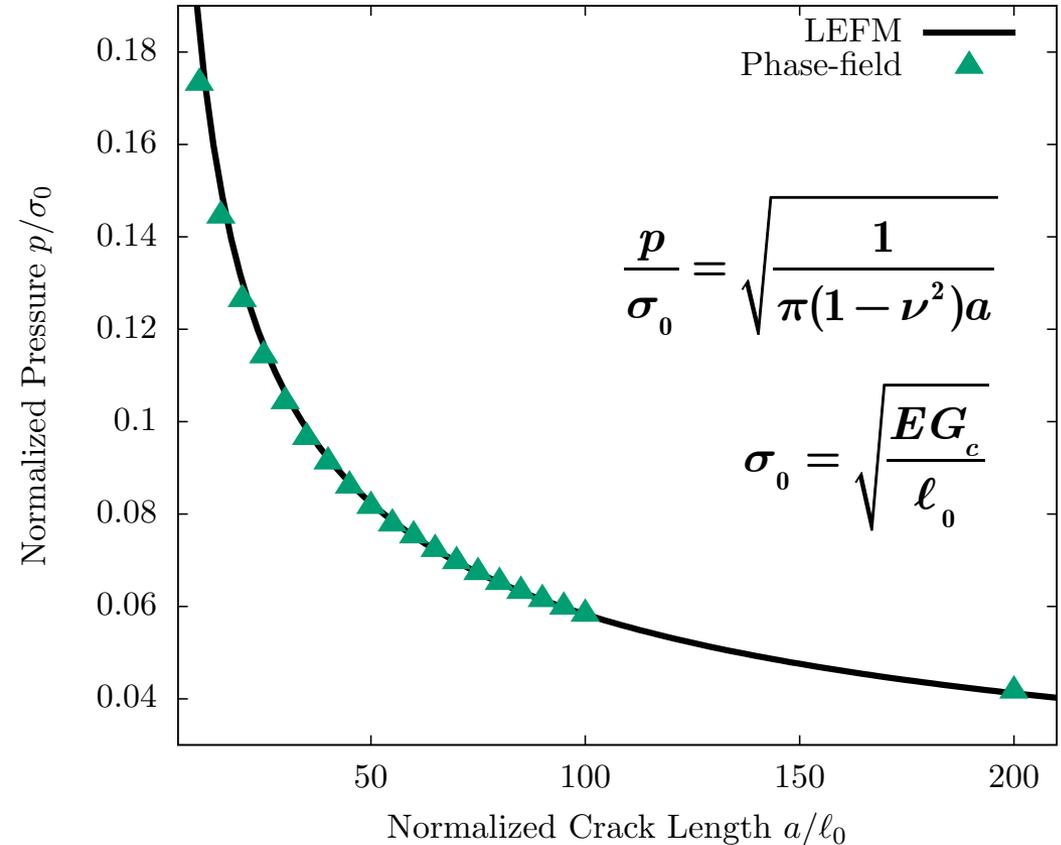
$u_x = 0$     $w_x = 0$



# Pressurized Center Crack



DtN Mapping on boundary elements



# Plane Strain Crack

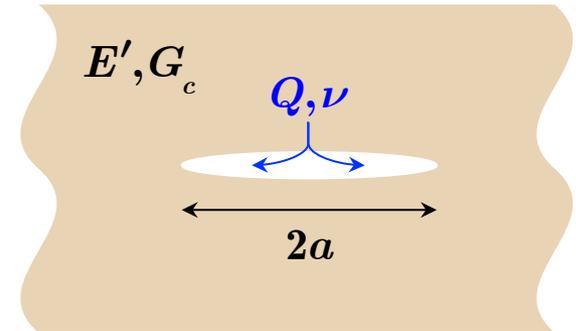
Two Regimes of Propagation:

$\mathcal{K} \rightarrow 0 \Rightarrow$  Viscosity Dominated  
 $\mathcal{K} \rightarrow \infty \Rightarrow$  Toughness Dominated

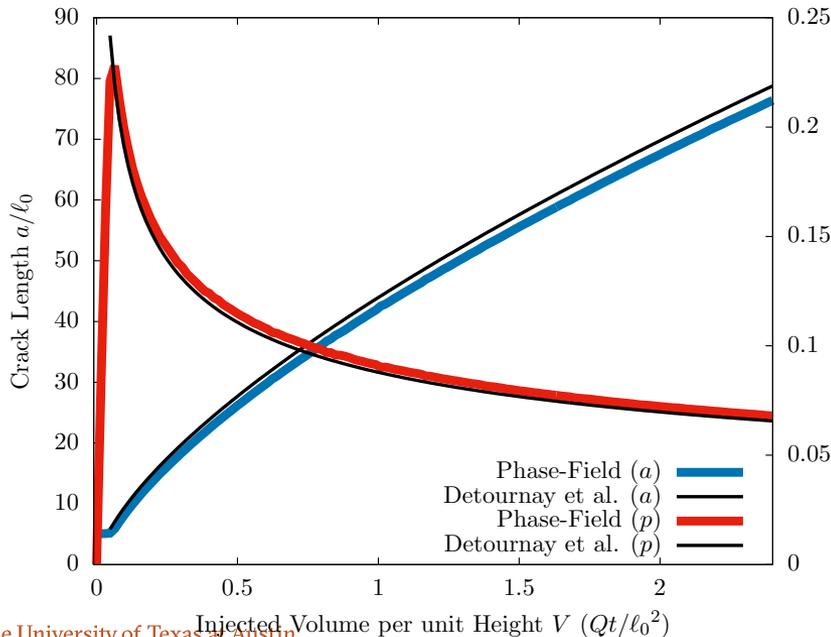
Dimensionless Toughness (Detournay):

$$\mathcal{K} = \frac{\left(4\sqrt{\frac{2}{\pi}}K_{Ic}\right)}{\left[E'\right]^3(12\nu)Q}^{1/4}, \quad K_{Ic} = \sqrt{G_c E'}$$

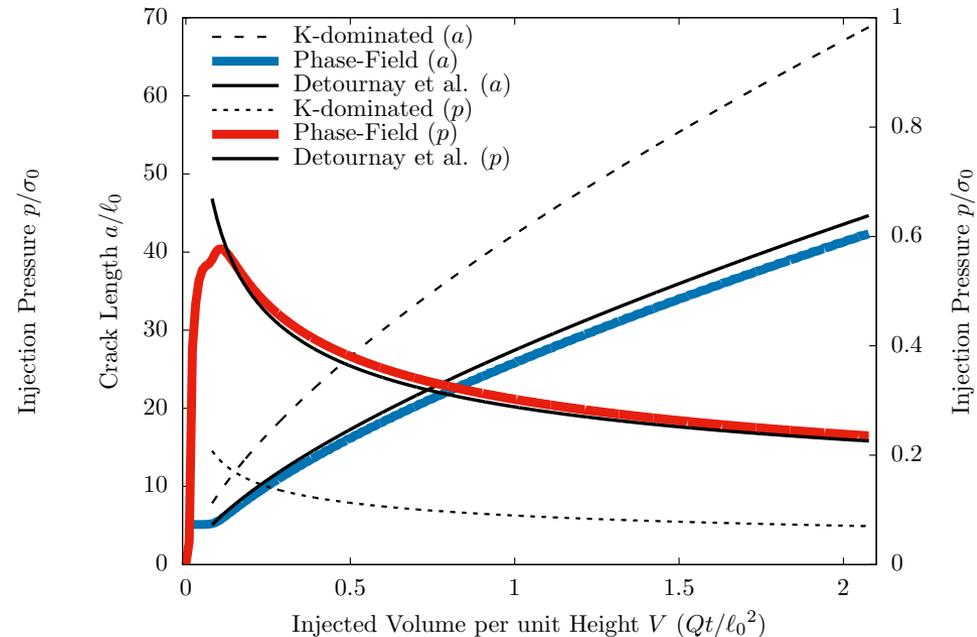
KGD crack geometry



TOUGHNESS DOMINATED REGIME

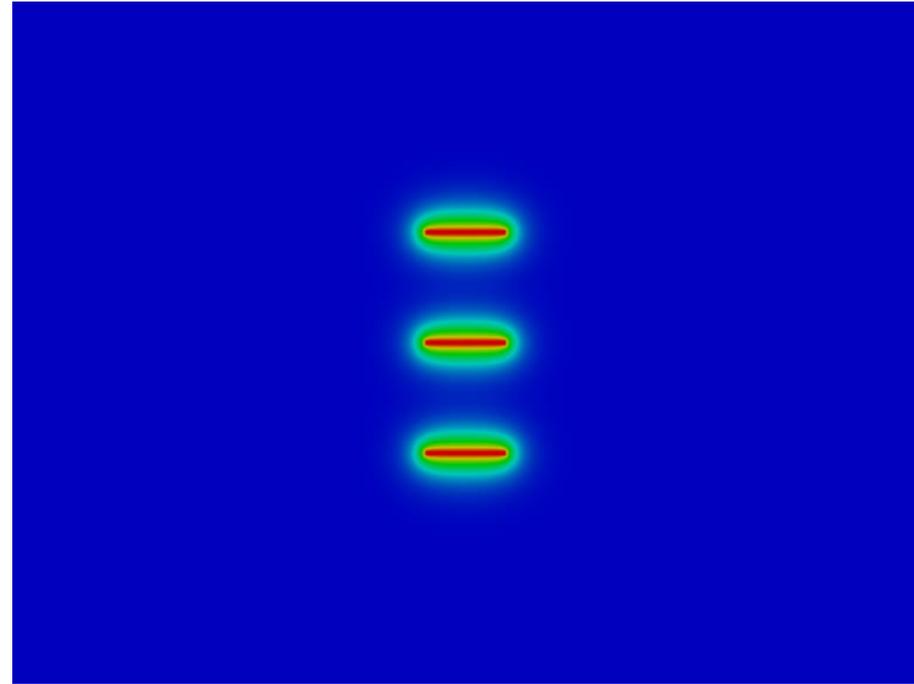
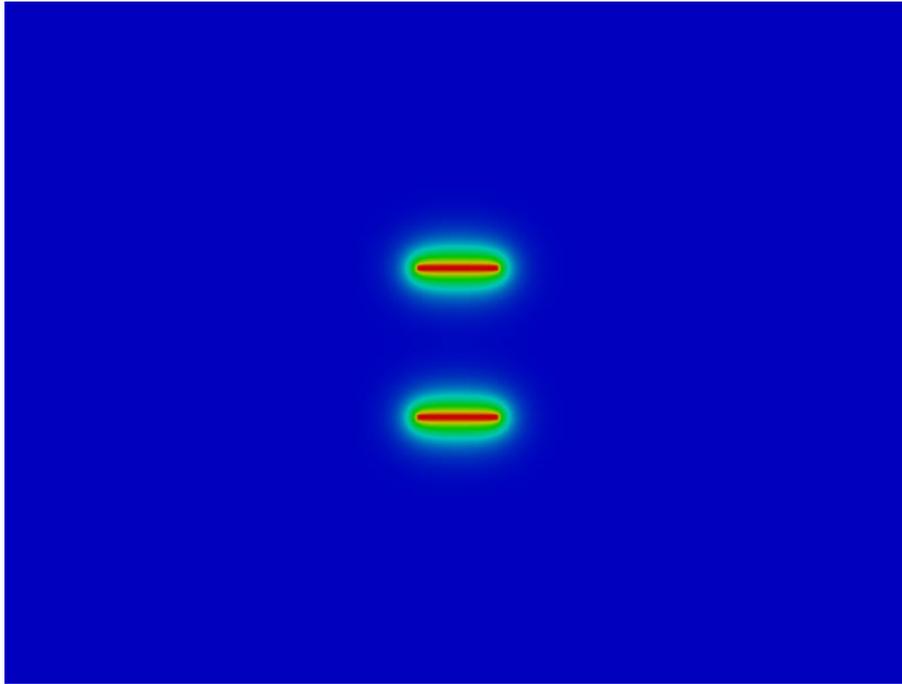


VISCOSITY DOMINATED REGIME



# Parallel Cracks

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# Merging Cracks

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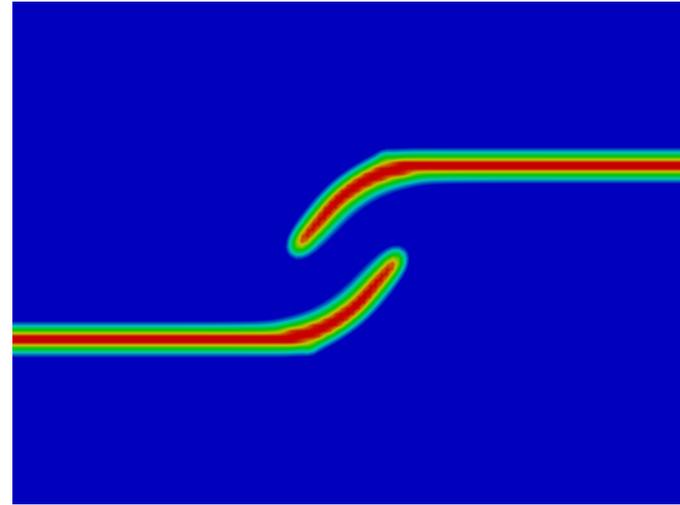
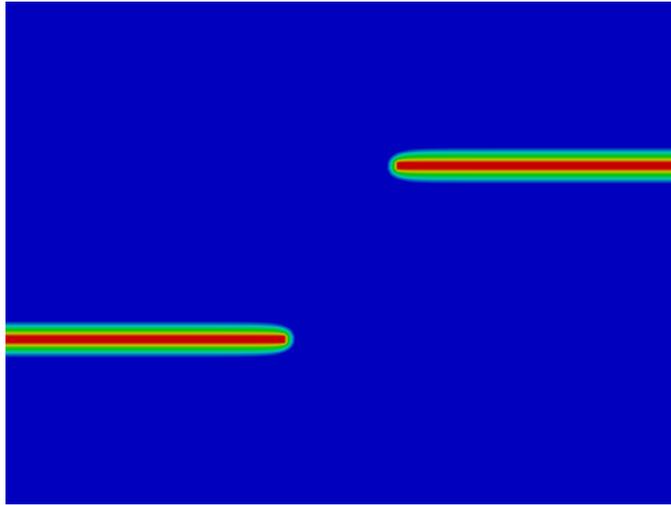
# Summary

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- **Cracks are represented by a diffuse phase-field and have been shown to be capable of representing interesting geometrical evolution.**
- **Thermodynamically consistent models have been developed using a balance law approach to model crack propagation fluid saturated poroelastic media**
- **The approach has been shown to compare favorably to several simple benchmark solutions.**

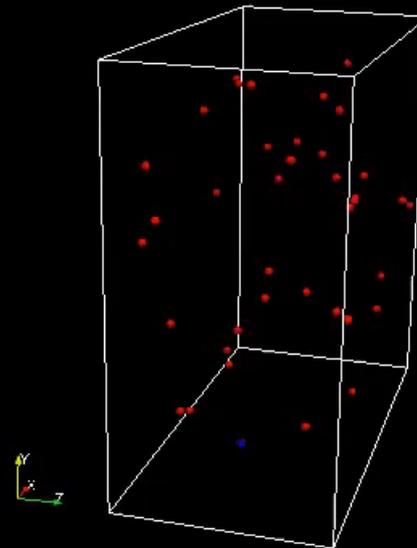
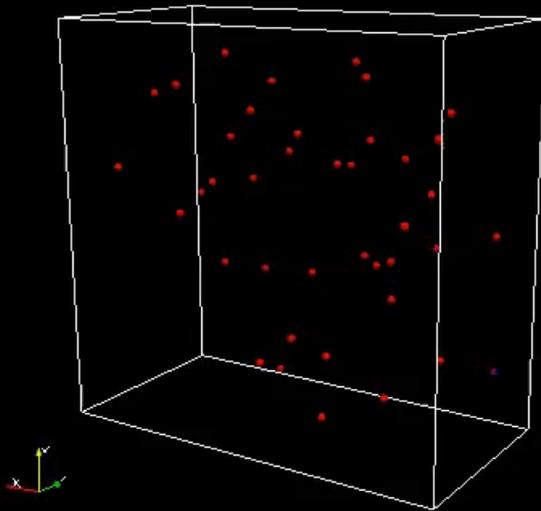
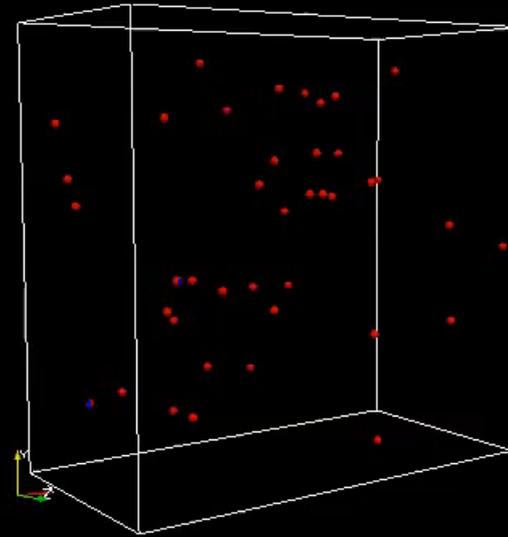
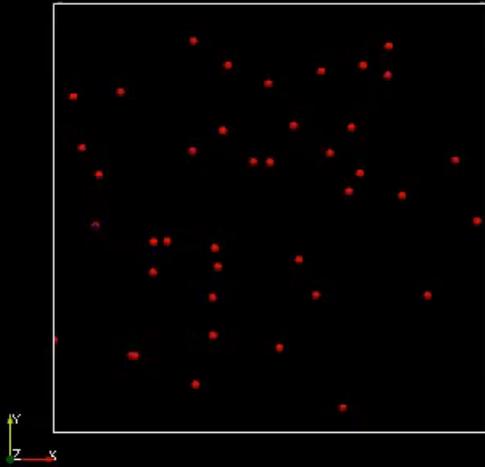
# Thank You for Your Attention

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- **Support from Statoil on this project is gratefully acknowledged.**

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# 3D Boiling

